

#### **Queensland Centre for Advanced Technologies (QCAT)**

Welcome, safety and CSIRO

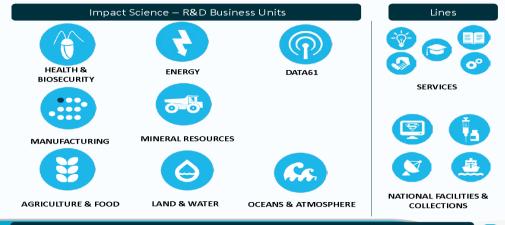
24 October 2016

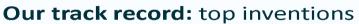
CSIRO ENERGY





## Current portfolio, CSIRO's lines of business









VACCINE











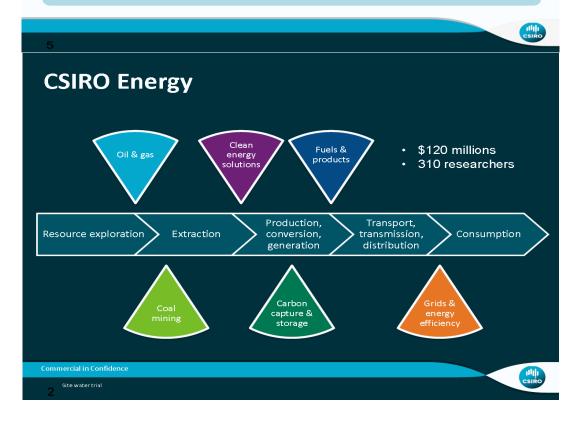
TOTAL
WELLBEING DIET

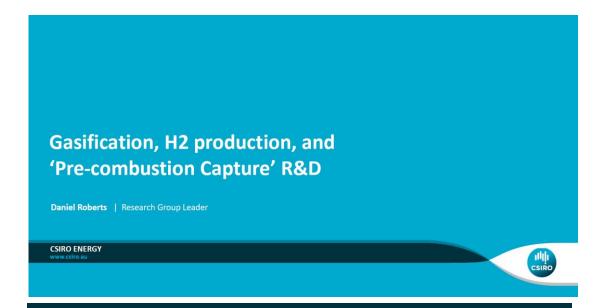








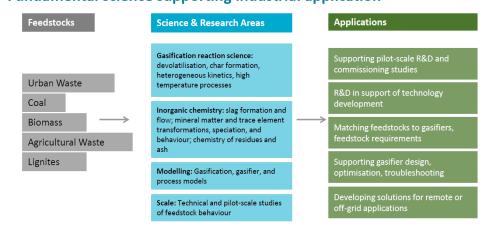




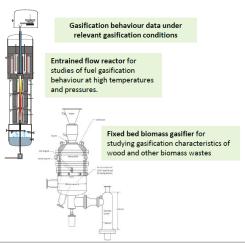
# Gasification of coal, biomass, and waste

## CSIRO Gasification Research

Fundamental science supporting industrial application



#### **CSIRO Gasification Research**



Supporting experiments allowing detailed interrogation of the gasification process







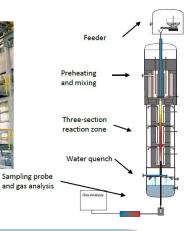
Characterisation of inorganic species to troubleshoot gasifier operation and manage disposal or reuse of residues



## **High Pressure Entrained Flow Reactor (PEFR)**

- Entrained-flow reactor
- Capable of 20 bar pressure. 1500°C wall temperature
- Coal feed rate of 1-5 kg/hr
- Gas mixtures of O<sub>2</sub>, CO<sub>2</sub>, H<sub>2</sub>O and N<sub>2</sub>
- · Adjustable sampling probe char and gas samples collected at different residence times (0.5-3s)







## **Mineral Matter in Gasification**

Slag viscosity, trace elements, and their impacts

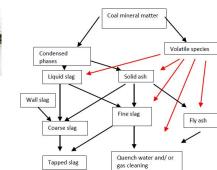






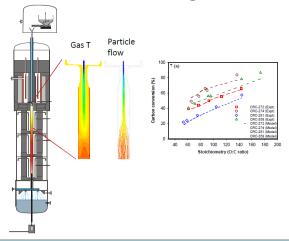
Volatile species (in syngas):

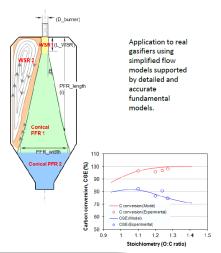
- requirements for syngas cleaning Condensed phases (slag, fly ash):
  - Syngas cleaning
  - · Operational: slag viscosity
  - Utilisation/handling of waste
  - · Physical & chemical properties: trace elements, leaching





#### **Gasification modelling**







#### Biomass and waste gasification

New facility for studying gasification behaviour of biomass

- Designed for forestry waste
- Well-suited for green waste

#### Research gasifier

- Can be integrated with gas-to-liquid test facilities
- Can be integrated with a 25kW microturbine for power generation

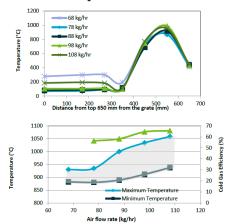




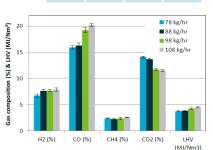




## **Gasifier operation**



Top air	Primary air	Secondary air	Total air (kg/hr)
0	39	29	68
0	44	34	78
0	48	40	88
0	53	45	98
0	58	50	108

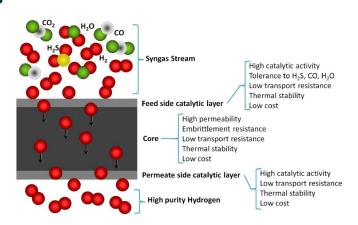


## **Metal membranes and membrane** reactors



#### **Metal membranes**

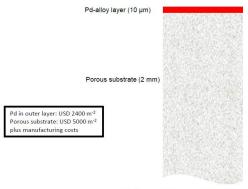
Separation of H<sub>2</sub> from gasification, reforming or ammonia-derived mixed gas streams





#### Supported Pd membrane

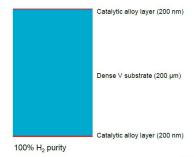
- Pd layer provides gas-tightness and H<sub>2</sub> separation
   Porous substrate provides strength



Must be >>10 µm to meet ISO14687

#### Layered V membrane

Pd layer provides H<sub>2</sub> separation
 V provides gas-tightness and strength



V in substrate: USD 180 m<sup>-2</sup> Catalytic layers: USD 100 m<sup>-2</sup> plus manufacturing costs

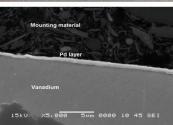


## **Layered V-based membranes**

- Embrittlement-resistant V-based alloy tube
  (natent pending)
- (patent pending)
   9.5 mm (3/8") OD
- · Catalytic surface coatings
- 300-350°C
- Very low cost (< \$2000/m<sup>2</sup> plus vessel), much cheaper than competing Pd-based membranes
- 100% pure H<sub>2</sub> (fuel cell compatible)









## **Industrial trials: Gas Reforming**

Coregas plant at Port Kembla











Page 1
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Nine Coetts.
(30) 4275



Hydrogen Purity ex CSIRO Trial Hydrogen Plant

a controller has been instand a thout any administration or connectors and shall not be reproduced section.

The following swepter collected by the laboratory have been analysed with the following results.

Laboratory Number: 16-015359

Call of Samples (South Call of Samples )

Samples (South Call of Samples )

Samples (South Call of Samples )



## Lignite gasification trials, 2015







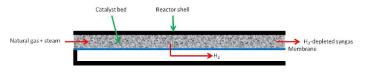
- Assessment of membrane performance for IGCC-CCS at EERC, Grand Forks ND
- · Lignite-derived syngas
- 30 bar, 350°C
- US DOE program



## Solar reforming, 2015



- Low temperature membrane reformer for solar-assisted  $\rm H_2$  production High methane conversion at 20 bar, 550°C (c.f. 800°C) In situ  $\rm H_2$  extraction (no downstream separation required Solar-thermal integration Partnership with ARENA



 $CH_4 + 2H_2O \rightleftharpoons CO_2 + 4H_2$ 



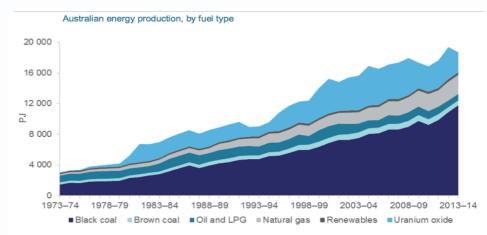
## Carbon dioxide storage

Lincoln Paterson | CSIRO Fellow 24 October 2016

ENERGY FLAGSHIP



## **Australian energy production**

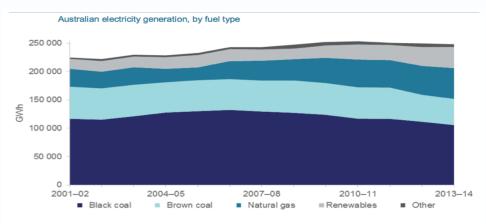


Source: Department of Industry and Science (2015) Australian Energy Statistics, Table J.

Carbon dioxide storage | Lincoln Patersor

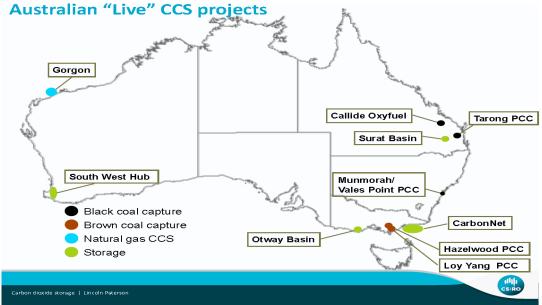


## **Australian electricity generation**



Source: Department of Industry and Science (2015) Australian Energy Statistics, Table O.

ıll||ı CSIRO



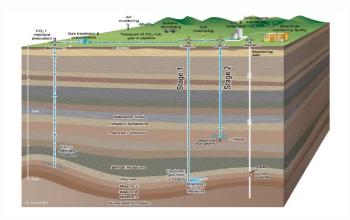
## Carbon dioxide storage

- CSIRO is currently working on:
  - Supporting the evaluation of Australian storage sites (especially the SW Hub, CarbonNet, and Surat Basin sites).
  - Modelling the injection of injected CO<sub>2</sub> plumes.
  - $\bullet$  Devising and applying methods to monitor the injected  ${\rm CO_2}$  to ensure it remains safe and secure.
  - Examining movement of groundwater in the vicinity of potential storage sites.
  - Engaging in international collaboration on CO<sub>2</sub> storage.
- CSIRO is a core research participant in the Cooperative Research Centre for Greenhouse Gas Technologies (CO2CRC) and the National Geosequestration Laboratory (NGL).

Carbon dioxide storage | Lincoln Paterson



## **CO2CRC Otway Project**



CO2 CRC



## **CO2CRC Otway Project**



CO2 CRC

Carbon dioxide storage | Lincoln Paterson

## Example of a CO<sub>2</sub> well



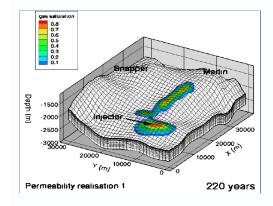
Carbon dioxide storage | Lincoln Paterson

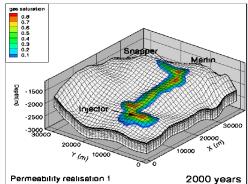


# Enhanced coal seam gas recovery with CO<sub>2</sub> at Liulin



## Reservoir simulation of injected CO<sub>2</sub>





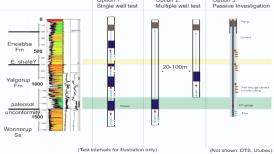
Carbon dioxide storage | Lincoln Patersor



## Designing CO<sub>2</sub> wells

Developing recommendations for well location, testing and instrumentation options for:

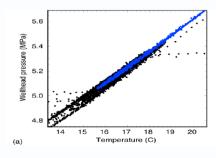
- Risk reduction and site characterisation, to define the CO<sub>2</sub> storage complex (containment and reservoir).
- Research and middle to long-term monitoring (e.g. deploy new instruments, implement new testing program, implement new injection techniques).



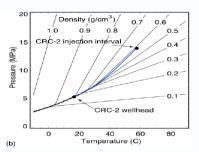
Carbon dioxide storage | Lincoln Paterson



#### Wellbore conditions



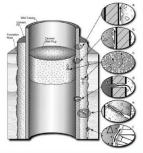
Wellhead (surface) conditions

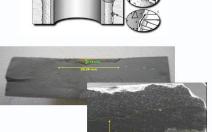


Pressure and temperature in a CO<sub>2</sub> well



## Integrity of wellbore cement





#### Cement degradation

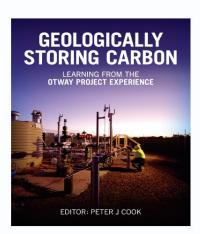
Cement (portlandite) Calcium Carbonat Amorphous silica gel

- Laboratory experiments of cement degradation
- · Reactive geochemistry simulations
- Predictions of well cement degradation under reservoir conditions

Carbon dioxide storage | Lincoln Paterson



## Otway project experience book



Publisher: CSIRO PUBLISHING

Hardback - August 2014

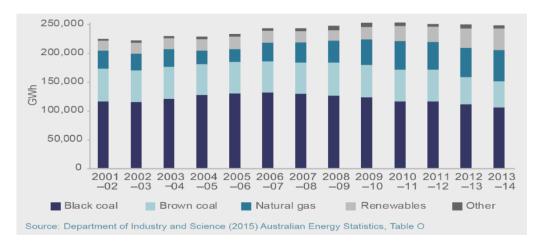
ISBN: 9781486302307

AU \$140.00

http://www.publish.csiro.au/pid/7317.htm



## **Electricity production in Australia**

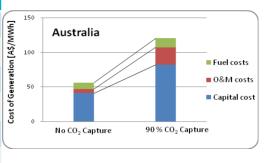


3 | Presentation title | Presenter name



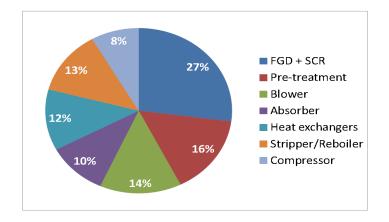
## Australian coal fired power stations

	Black coal	Brown coal
Average efficiency [% HHV]	35.6	25.7
CO <sub>2</sub> emission [tonne/MWh]	0.9	1.3
SO <sub>2</sub> concentration [g/m³]	0.5 – 1.7	0.2 – 0.7
$NO_x$ concentration [g/m <sup>3</sup> ]	0.4 – 1.5	0.2 – 0.4
Particulate matter [mg/m³]	10 – 100	10-60
Flue gas temperature [°C]	120	180
	120	180



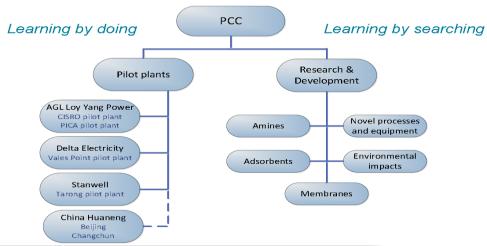
Data derived from CCSD – technology assessment report 62

## **PCC** equipment costs overview





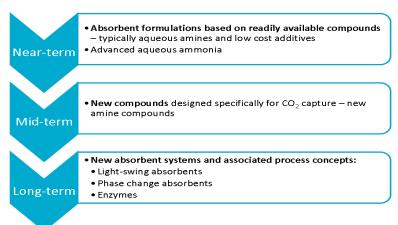
#### **CSIRO's PCC program**





## CSIRO's chemical absorbent research program

#### **Graeme Puxty**





#### **Rotating liquid sheet contactor**

Leigh Wardhaugh

#### **Basic principles**

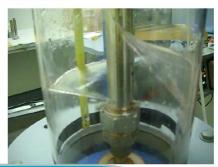
- Surface area of stabilized liquid sheet greater than that resulting droplets
- Rotating liquid surface proven experimentally to pump gas
- Centrifugal + liquid pumping force creates interfacial area

#### **Advantages**

- · Higher gas velocities possible
- · Liquid entrainment significantly reduced
- Suitable for viscous solvents

#### Challenges

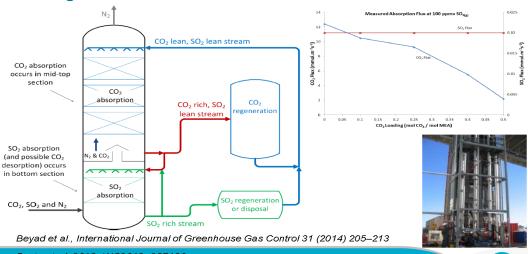
- · Scale-up to commercial scale
- · Liquid residence time low



Wardhaugh et al, Greenhouse Gas Sci Technol. 5:198–209 (2015)



# Integrated single stream $SO_2$ and $CO_2$ capture Ashleigh Cousins



Puxty et al. 2012, WO2012\_097406



#### Aqueous ammonia

#### Hai Yu

- Indestructible liquid absorbent
- Chemical well-known to electricity industry
- Suited for "contaminated" feed gases
- Fertiliser by-product
- Product CO<sub>2</sub> at elevated pressure
- Technical feasibility demonstrated in pilot plant but no cost advantage
- > Addressing challenges:
  - ☐ Mass transfer promotion, temperature increase
  - Vapour suppressors
  - Further integration of pretreatment and water wash
  - □ Process design



## Solid sorbent CO<sub>2</sub> capture unit at Vales Point

Ramesh Thiruvenkatachari

#### > Objective

- ☐ Evaluate the stability of honeycomb CF composite monolithic adsorbents using the real flue gas
- ☐ Understand the effect of real flue gas characteristics on the operation and performance of the CO<sub>2</sub> capture unit



#### > Results

- ☐ Excellent stability to real flue gas over 200 experiments
- ☐ CO<sub>2</sub> adsorption efficiency consistently over 98%
- $\square$  CO<sub>2</sub> desorption efficiency between 90-95%
- ☐ Near complete removal of SO<sub>2</sub> and NO<sub>x</sub>
- ☐ Could be pretreatment unit for amine based PCC



Thiruvenkatachari et al. IJGGC 42 (2015) 415–423

# Emission issues addressed via integrated approach

**Merched Azzi** 



- Absorbent degradation in absorber
- Absorbent degradation in desorber

#### 2. Emission analysis

- · Estimation of concentrations using process models
- · Actual measurements in pilot plants

#### 3. Dispersion

- Smog chamber to investigate atmospheric degradation
- Updating dispersion models with atmospheric chemistry







## Piloting PCC Technologies in Australia



Preparing for deployment
- Next-generation PCC

CCS demo's



#### **Pilot plant summary**

**Aaron Cottrell** 

Plant	Loy Yang	Vales Point	Tarong	PICA
Solvent	Amine	Ammonia/ Amine	Amine	Amine
Flue gas source	Brown coal	Black coal	Black coal	Brown coal
Scale	50 kg/hr CO <sub>2</sub>	300 kg/hr CO <sub>2</sub>	100 kg/hr CO <sub>2</sub>	50 kg/hr CO <sub>2</sub>
Focus	Solvent benchmarking	Ammonia operation	Process optimisation	Duration evaluation
Other activities	Emission study Combined CO <sub>2</sub> /SO <sub>2</sub> capture	Pressurised absorption Solar thermal integration	Pressurised stripping Corrosion Degradation	



## Solar thermal energy for absorbent regeneration

James McGregor

- Avoiding interface with existing steam cycle
- More effective in terms of CO<sub>2</sub>emission reduction
- > Introduction of flexibility into the capture process

Pilot plant at Vales Point power station

- Integrated with existing PCC pilot plant
- > 65 kW<sub>th</sub> solar array







http://arena.gov.au/files/2015/08/3-A006-Final-Report-and-Lessons-Learnt.pdf



## **PICA** project

**Aaron Cottrell** 

#### Project aims:

- > 40% lower cost compared to the MEA base case
- ☐Advanced packing materials, liquid absorbent and
- Long-term performance evaluation both IHI Corporation and CSIRO developed technologies
- Supporting large-scale CCS as an affordable, secure and environmentally benign option for power generation







PCC IHI CSIRO AGL



#### **Process Development Facility**

**Dan Maher** 



- Located at Newcastle Energy Technology Labs
- Scale between Lab bench scale and Pilot scale
- Modular design
- Flexible operation
- Ventilated & bunded space
- "Controlled" environment



#### **Outlook for PCC in Australia – Next steps**

- Qualification of new liquid absorbents towards deployment
  - Formulations and designer amines
  - · Optimisation of process design
- Development of SO<sub>2</sub>/CO<sub>2</sub> process concept
- Focus on process and equipment innovation
- Solar thermal integration demonstration
- Continued efforts in next-gen technologies
  - Adsorbents, membranes
  - Advanced liquid absorbent systems

